

**MONTGOMERY & STIEFEL**

**Ice and Refrigeration in**

**Connection with the Central Station**

**Electrical Engineering**

**B. S.**

**1912**



THE UNIVERSITY


OF ILLINOIS

LIBRARY

1912  
M76







Digitized by the Internet Archive  
in 2013

<http://archive.org/details/icerefrigeration00mont>



**ICE AND REFRIGERATION**  
**IN CONNECTION WITH THE CENTRAL STATION**

**BY**

**HARRY EDGAR MONTGOMERY**  
**AND**  
**IRA BROKAW STIEFEL**

-----  
**T H E S I S**

**FOR THE**

**DEGREE OF BACHELOR OF SCIENCE**

**IN**

**ELECTRICAL ENGINEERING**

-----  
**COLLEGE OF ENGINEERING**

**UNIVERSITY OF ILLINOIS**

**1912**



1912

M76

UNIVERSITY OF ILLINOIS

May 16, 1902

THIS IS TO CERTIFY THAT THE THESIS PREPARED UNDER MY SUPERVISION BY

HARRY EDGAR MONTGOMERY & IRA BROKAW STIEFFEL

ENTITLED ICE AND REFRIGERATION IN CONNECTION WITH THE CENTRAL  
STATION

IS APPROVED BY ME AS FULFILLING THIS PART OF THE REQUIREMENTS FOR THE

DEGREE OF BACHELOR OF SCIENCE IN ELECTRICAL ENGINEERING

*Edw. H. Mallo*  
Instructor in Charge

APPROVED:

*E. H. Mallo*

HEAD OF DEPARTMENT OF ELECTRICAL ENGINEERING.

1. *General*

2. *General*

3. *General*

4. *General*

5. *General*

6. *General*

7. *General*

8. *General*





# TABLE OF CONTENTS.

	page.
I. INTRODUCTION. . . . .	1
II. VARIOUS REFRIGERATING SYSTEMS. . . . .	2
Ammonia . . . . .	2
Compression. . . . .	2
Dry . . . . .	2
Flooded . . . . .	2
Absorption . . . . .	3
Sulphur Dioxide . . . . .	3
Other Mediums . . . . .	4
Methods of Freezing . . . . .	4
III. CALCULATIONS FOR PROPOSED PLANTS. . . . .	6
Sample Calculations . . . . .	6
Compression Motor Driven Plant. . . . .	7
Case I . . . . .	7
Case II. . . . .	9
Case III . . . . .	10
Absorption System . . . . .	12
Case IV. . . . .	12
IV. ACTUAL DATA. . . . .	14
Absorption Plant. . . . .	14
Compression Plant . . . . .	16
Natural Ice . . . . .	18
V. CONCLUSIONS . . . . .	19
VI. APPENDIX . . . . .	24



## ICE AND REFRIGERATION IN CONNECTION WITH THE CENTRAL STATION.

### I. INTRODUCTION.

It is the purpose of the writers to give a method of determining the approximate cost of operating an ice and refrigeration plant in connection with the central station, and to show that it is a paying proposition for the central station manager. Only the more common refrigeration systems, namely, compression and absorption, with ammonia as a medium, have been discussed in detail. Some data has been gathered from technical articles, some from books of commercial plants, but most of it is purely theoretical. Estimates on the cost of machinery and apparatus have been procured from some of the leading manufacturing firms, namely, The York Manufacturing Company, and the Carbondale Machine Company. Actual data on the cost of operating such plants is very hard to obtain. In most cases where the refrigeration system is operated with the central station, the books of the two departments are not kept separate; and those companies who do keep their books separate are very reluctant about giving out information, except in a general way. Therefore, it has been necessary to make certain assumptions and to compare the results obtained with the actual data at hand.





## II. VARIOUS REFRIGERATING SYSTEMS.

The ammonia system, being the most common, will first be discussed. Of this class, the compression system is the more common and consists fundamentally of four parts. First, there is a compressor, which is usually a steam or motor driven unit. Generally this is single acting, the compression taking place in the head end, the pressure being about one hundred and eighty pounds per square inch. The compressor discharges the ammonia into the cooling coils, which are generally surface cooled by running water, and in these coils the gas becomes a liquid. The liquid passes thru an expansion valve, which is the third step of the cycle. This is a wire-drawing process in which the pressure is reduced to about ten or fifteen pounds per square inch. In passing the valve the liquid ammonia becomes a gas, due to expansion, and absorbs heat during its passage thru the expansion or freezing coils, thereby completing the cycle.

There are two compression systems in general use, the dry and the flooded. The main difference between the two is the condition of the ammonia in the expansion or freezing coils. In the dry system ammonia gas alone is present, while in the flooded liquid ammonia is mixed with the gas. The dry system was originally employed, but the advantages claimed for the flooded system are bringing the latter into more general use.

In the flooded system the freezing coils contain liquid ammonia and gas at all times, but not in any definite proportion. An accumulator, which separates the liquid ammonia from the gas,





is placed between the coils and the intake for the compressor. Some of the liquid ammonia is often allowed to enter the compressor, thus keeping down the heat, and dispensing with the water jacket around the compressor cylinder. The advocates of the flooded system claim that the heat absorbing surface of the coils will transmit about seventy-five percent more heat per square foot of surface per degree difference in temperature of the mediums when there is liquid on both sides of the coils than when operated with gas on the inside and liquid on the outside.

The absorption system is similar to the compression system in that there are four distinct steps. The generator takes the place of the compressor, and the ammonia gas, instead of being compressed mechanically, is compressed by heating. The gas, after leaving the freezing coils, enters the absorber, where it is taken up by the water. The aqua ammonia solution is then pumped into the generator, where it is boiled by means of steam; usually the exhaust from engines or auxiliaries being used. The ammonia gas is driven off and lead into the cooling coils, the remainder of the cycle being completed in the same manner as in the compression system.

The Sulphur Dioxide system has the same cycle as the compression system described, the difference being that sulphur dioxide is used instead of ammonia as a medium. The machine is very compact, the entire cycle of the medium being enclosed in a hermetically sealed case from which the air has been exhausted. Valves are eliminated in this machine by the use of annular openings in the shaft and trunnions which support the compressor.



A good idea of the system can be obtained from the cross section of the machine shown in Figure I. The outside appearance is that of a huge dumb-bell, the two ends being hollow globes, one of which contains the compression cylinder.

This cylinder is hung in a vertical position from a shaft rigidly attached to, and running lengthwise thru the machine. To this shaft is fitted a crank to which the piston is attached. The entire mechanism revolves, except the cylinder which is kept upright by a counter-weight. The globe, which contains the cylinder, takes the place of the cooling coils and is partly immersed in cooling water.

The second globe, which takes the place of the freezing coils, runs partly immersed in the liquid to be cooled. Inside of the shaft is a small tube thru which the liquid refrigerant flows into the second globe. Here it absorbs heat, and returns to a gaseous state and as a gas is lead back thru the hollow shaft to the compression cylinder.

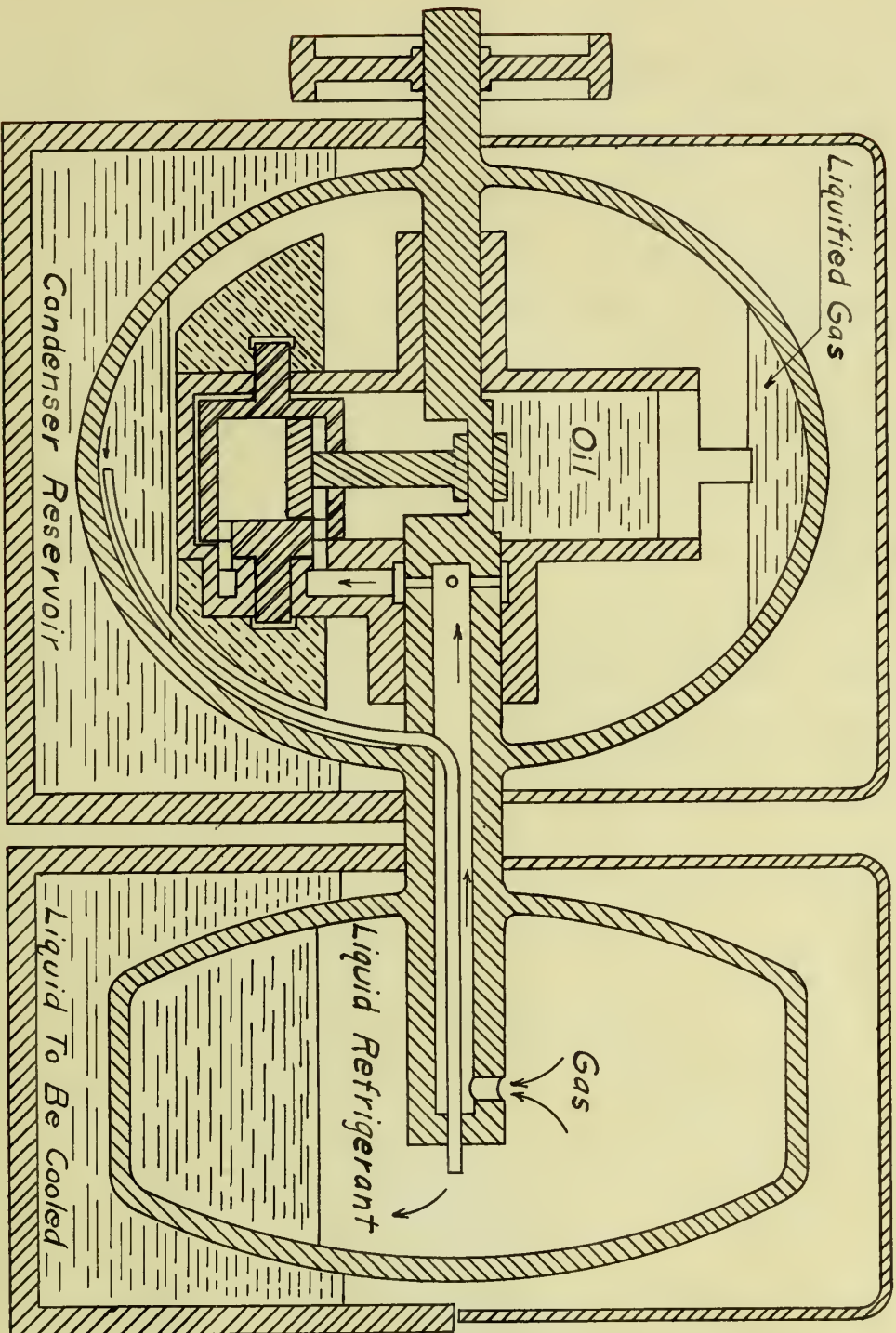
Several mediums, which may be used are Ether, Sulphuric Ether, Methylic Ether, Carbonic Acid, and Pictet Fluid. Most of these have been used experimentally only, and, as data is not available, a further description will not be taken up.

Either the plate or the can system of freezing is generally used. By the plate system the ice is frozen in huge flat plates, which are afterwards sawed into commercial sized cakes. In the second system the ice is frozen in upright cans placed in parallel rows in the brine tank. The inside dimensions of these cans are those of an ordinary commercial cake.





*Sketch of  
Sulphur Dioxide  
Machine.*



*Figure I.*





### III. CALCULATIONS FOR PROPOSED PLANTS.

In these calculations entirely theoretical plants have been assumed. In the operating expenses of the ice plants, the increase in fuel consumption has been the only charge for power. The cost of labor, interest, insurance, and depreciation on the machinery and buildings has been considered in the final cost per ton of product.

In the different cases, the year has been divided into seasons and a theoretical load curve drawn for each. The same efficiency curve was taken for the different units. Steam consumption curves were assumed for the various systems of operating; the steam engines being taken as ninety-two percent efficient at all loads. From this assumed data the steam consumption for the different seasons has been found as shown in these sample calculations:-

Example:- - Case I. Table I. Line 4.

K.W. and Hours from load curve.

$$\text{Percent load on Generator. } \frac{260}{300} = 86.6\%$$

$$\text{Efficiency from efficiency curve. } = 94.5\%$$

$$\text{Input} = \frac{\text{K.W.}}{\text{Eff.}} = \frac{260}{.945} = 275 \text{ K.W.}$$

$$\text{B.H.P.} = \frac{\text{Input}}{.746} = \frac{275}{.746} = 369 \text{ H.P.}$$

$$\text{Efficiency of Engine} = 92\%$$

$$\text{I.H.P.} = \frac{\text{B.H.P.}}{\text{Eff.}} = \frac{369}{.92} = 401 \text{ H.P.}$$

$$\text{Percent of total load} = \frac{\text{I.H.P. load}}{\text{I.H.P. Engine.}} = \frac{401}{460} = 87.2\%$$



Steam Consumption per I.H.P. Hr. from curve = 14.5#.

Total Steam Consumption = I.H.P. x steam consumption per

I.H.P. Hr. x No. Hours. = 401 x 14.5 x 1 = 5830# per Hr.

# CASE I.

A Twenty ton compression system ice plant, motor driven, is operated in connection with a Five hundred kilo-watt plant. Two units are employed, a Three hundred kilo-watt generator, driven by a Four hundred and sixty I.H.P. compound condensing Corliss engine, and a Two hundred kilo-watt generator, driven by a similar engine of Three hundred I.H.P. The engines operate under steam pressure of one hundred pounds gage on the high side and four and three fourths pounds absolute back pressure, with twenty per cent cut-off.

Data taken from Tables I-VIII of Appendix:-

	1st season.	2nd season.	3rd season.	4th season.
Steam consumption with ice plant.	168320	185940	166776	153140
Steam consumption without ice plant.	<u>150730</u>	<u>142065</u>	<u>119890</u>	<u>136210</u>
Increased steam consumption.	17590#	43875#	46886#	16930#

Total steam consumption per quarter equals steam consumption per day times days per quarter.

1st season.	17590 x 89 =	1565510#
2nd season.	43875 x 92 =	4036500#
3rd season.	46886 x 92 =	4313512#





$$\text{4th season.} \quad 16930 \times 91 = \frac{1540630\#}{11456152\#}$$

Assume quality of steam as 98%

Coal = 11000 B.t.u. per lb.

Feed water temperature = 200°.

$$\text{Factor of evaporation} = \frac{q + xr - qf}{966.3} =$$

$$\frac{308.5 + .98(880.75) - 168}{966.3} = \frac{1004.5}{966.3} = 1.04$$

Boiler efficiency = 60%.

$$\frac{1100 \times .6}{11456152} = 6.57\# \text{ water evaporated per pound coal consumed.}$$

$$\frac{1004.5}{6.57} = 1743710\# \text{ coal per year} = 871.85 \text{ Tons.}$$

Cost of coal = \$2.00 per ton.

$$871.85 \times \$2.00 = \$1743.70 \text{ per year.}$$

#### Investment:-

Cost of buildings, estimated. \$10000.00

Cost of machines, including motors. 12125.00  
\$22125.00

Interest, depreciation, and insurance = 15%.

$$\$22125 \times .15 = \$3318.75$$

#### Operating expenses:-

Interest and depreciation. \$3318.75

Coal 1743.70

Labor, Two men for one year @ \$2.00 per day. 1500.00

General Expenses. 300.00

Total operating costs. \$6862.45

Ice made, calculated on percent load at which ice machines were operated.

First season. Half load. 890 Tons.

Second season. Full load. 1840 Tons.



Third season.	One fourth over load.	2300 Tons.
Fourth season.	Half load.	<u>910 Tons.</u>
Total Ice made during year.		5940 Tons.
$\frac{6862.45}{5940} = \$1.156 = \text{cost per ton of ice at platform.}$		

## CASE II.

For the second case, a compression system, motor driven, ice plant of Forty ton capacity is operated with a One thousand kilo-watt plant. In the power plant two units are used, namely, one Three hundred kilo-watt generator, driven by a Four hundred I.H.P. compound condensing Corliss engine, and one Seven hundred kilo-watt generator, driven by a similar engine of one Thousand I.H.P. Other conditions are the same as in Case I, except that the ice plant is shut down during the winter months.

Data taken from Tables I-VI of Appendix:-

	2nd season.	3rd season.	4th season.
Steam consumption with ice plant.	363690	366150	379430
Steam consumption without ice plant.	<u>316030</u>	<u>270010</u>	<u>330860</u>
Increased steam consumption.	47660#	96140#	48570#

Total steam consumption per quarter equals steam consumption per day times days per quarter.

2nd season.	47660 x 92 =	4384720#
3rd season.	96140 x 92 =	8844880#
4th season.	48570 x 91 =	<u>4419870#</u> 17649470#.

Taking, as in Case I, 6.57 pounds water evaporated per





pound of coal consumed.

$$\frac{17649470}{6.57} = 2686373\# \text{ coal per year} = 1343.2 \text{ Tons.}$$

Cost of coal = \$2.00 per ton.

$$1343.2 \times \$2.00 = \$2686.40 \text{ per year.}$$

Investment:-

Cost of buildings, estimated.	\$15000.00
-------------------------------	------------

Cost of machines, including motors.	20100.00
	<u>\$35100.00</u>

Interest, depreciation, and insurance = 15%.

$$\$35100.00 \times .15 = \$5265.00$$

Operating expenses:-

Interest and depreciation.	\$ 5265.00
----------------------------	------------

Coal.	2686.40
-------	---------

Labor, Three men for one year @ \$2.00 per day.	2200.00
---	---------

General Expenses.	600.00
-------------------	--------

Total operating costs.	<u>\$10751.40</u>
------------------------	-------------------

Ice made, calculated on percent load at which ice machines were operated.

Second season.	Half load.	1840 Tons.
----------------	------------	------------

Third season.	Full load.	3680 Tons.
---------------	------------	------------

Fourth season.	Half load.	1820 Tons.
----------------	------------	------------

Total ice made during year.		<u>7340 Tons.</u>
-----------------------------	--	-------------------

$$\frac{10751.40}{7340} = \$1.465 = \text{cost per ton of ice at platform.}$$

### CASE III.

The plant of Case I, with the same load curves was assumed, changing the engines from compound condensing Corliss to comp-



ound non-condensing Corliss. A motor driven, compression system, ice plant of the same capacity was operated, and the cost per ton calculated in the same manner as before.

Data taken from Tables I-VIII of Appendix:-

	1st season.	2nd season.	3rd season.	4th season.
Steam consumption with ice plant.	271320	297900	269230	247290
Steam consumption without ice plant.	<u>243080</u>	<u>228880</u>	<u>193670</u>	<u>219720</u>
Increased steam consumption.	28240#	69020#	75560#	27570#

Total steam consumption per season equals total steam consumption per day times days per season.

1st season.	28240 x 89 = 2513360#
2nd season.	69020 x 92 = 6349840#
3rd season.	75560 x 92 = 6951520#
4th season.	27570 x 91 = <u>2508870#</u> 18323590#

Taking, as in Case I, 6.57 pounds water evaporated per pound coal consumed.

$$\frac{18323590}{6.57} = 2790000\# \text{ coal per year} = 1395 \text{ Tons.}$$

Cost of coal = \$2.00 per ton.

$$1395 \times \$2.00 = \$2790.00 \text{ per year.}$$

Investment:-

Cost of buildings, estimated.	\$10000.00
Cost of machines, including motors.	<u>12125.00</u> \$22125.00

Interest, depreciation, and insurance = 15%.

$$\$22125.00 \times .15 = \$3318.75$$





Operating expenses:-

Interest and depreciation.	\$3318.75
Coal.	2790.00
Labor, Two men for one year @ \$2.00 per day.	1500.00
General expenses.	300.00
Total operating expenses.	<u>\$7910.75</u>

Ice made, calculated on percent load at which ice machines were operated.

First season.	Half load.	890 Tons.
Second season.	Full load.	1840 Tons.
Third season.	One quarter over load.	2300 Tons.
Fourth season.	Half load.	<u>910 Tons.</u>
		5940 Tons.

$$\frac{7910.75}{5940} = \$1.33 = \text{cost per ton of ice at platform.}$$

CASE IV.

An absorption system ice plant of Twenty tons capacity working under Two pounds gage pressure, is operated with the power plant of Case III, instead of the compression plant. The cost per ton is calculated in the same manner as before, the ice plant being charged with the increased coal consumption due to back pressure.

Data taken from Tables I-IV of Appendix.

	1st season.	2nd season.	3rd season.	4th season.
Steam consumption with ice plant.	257660	242480	205375	233040
Steam consumption without ice plant.	<u>243080</u>	<u>228880</u>	<u>193670</u>	<u>219720</u>
Increased steam consumption.	14580#	13600#	11705#	13320#



Total steam consumption per season equals steam consumption per day times number of days per season.

1st season.	14580 x 89 = 1297620#
2nd season.	13600 x 92 = 1251200#
3rd season.	11705 x 92 = 1076860#
4th season.	13320 x 91 = <u>1212120#</u> 4837800#

Taking, as in Case I, 6.57 pounds water evaporated per pound of coal consumed.

$$\frac{4837800}{6.57} = 736350\# \text{ coal per year} = 368.18 \text{ Tons.}$$

Cost of coal = \$2.00 per ton.

$$368.18 \times \$2.00 = \$736.36 \text{ per year.}$$

Investment:-

Cost of buildings, estimated.	\$10000.00
Cost of machines, including motors.	12125.00
Additional cost of erection over compression.	<u>2500.00</u> \$24625.00

Interest, depreciation, and insurance = 15%.

$$\$24625.00 \times .15 = \$3700.00$$

Operating expenses:-

Interest and depreciation.	\$3700.00
Coal.	736.36
Labor, Two men for one year @ \$2.00 per day.	1500.00
General expenses.	300.00
Assume 10 K.W. per hr. @ 2¢ per K.W.	<u>1752.00</u>
Total operating costs.	\$7988.36

Ice made, calculated on percent load at which machines were operated.





First season.	Half load.	890 Tons.
Second season.	Full load.	1840 Tons.
Third season.	One fourth over load.	2300 Tons.
Fourth season.	Half load.	<u>910 Tons.</u>
Total ice made during year.		5940 Tons.
$\frac{7988.36}{5940} = \$1.345 = \text{cost per ton of ice at platform.}$		

#### IV. ACTUAL DATA.

##### ABSORPTION SYSTEM.

The data of this plant was obtained directly from the books of the company, whose name, by their request, is with-held. This data covers a period of one year, Oct. 31, 1910 to Oct. 31, 1911. The plant under discussion is a Voigt absorption system of Twenty tons capacity, and is operated in connection with a Three hundred kilo-volt-ampere plant. Ice was made during the winter as sold, very little being stored. A refrigerating room, having a capacity of four hundred barrels is part of the building.

The ammonia and brine pumps are steam driven, the rest of the auxiliaries being driven by induction motors.

The cost per ton at platform in this plant has been determined from the operating expenses, which include coal, water, power, labor, repairs, and miscellaneous expenses. In calculating the net earnings interest, insurance, and taxes have been included with the operating expenses to make up the total cost, no accumulating depreciation charges being made.



The following tables show the data as taken from the books:-

Operating costs.

Month.	Wages.	Coal.	Water.	Power.	Supplies.	Repairs.	Misc.	Exp.
Nov.	\$ 20.00	\$ 20.78	\$30.35	\$	\$	\$ 5.28	\$ 5.51	
Dec.	20.00	8.95	28.06					
Jan.	20.00	7.52	32.90				4.23	
Feb.	64.50	19.60	31.00	1.80				
Mar.	49.13	31.98	31.00	6.40		14.00	17.10	
Apr.	65.00	60.00	31.50	30.00				
May.	90.00	96.60	34.00	56.00		21.46		
June.	197.41	149.45	30.00	133.20	30.00		23.27	
July.	228.04	144.50	31.00	130.80	35.00		24.60	
Aug.	189.90	144.19	31.00	130.80	35.00		65.31	
Sept.	176.90	116.25	30.00	115.20	30.00			
Oct.	114.85	61.60	25.00	96.06	30.00			

General Data.

Month	Ice Pulled	Shrinkage	Oper. cost per ton ice.	Gross Price received.
Nov.	190500#	1850#	\$ .724	\$6.33
Dec.	84900	0	.598	5.60
Jan.	63700	0	1.890	6.00
Feb.	168300	0	1.440	6.00
Mar.	256380	280	1.568	6.00
Apr.	500000	305	1.000	7.00
May.	839540	2360	.952	6.20
June.	1243320	3840	1.016	6.20
July.	1222700	3110	.950	6.00
Aug.	1227860	2680	.895	6.40
Sept.	975430	3000	.880	6.00
Oct.	559978	6290	1.960	6.40
	7332608#		Av. =\$1.156	

Average price per ton at platform. \$6.00

Delivery cost per ton. \$1.50

Cost per ton to load on cars. \$ .24

Amount of ice loaded in car load lots, in pounds 78300.

Earnings.

Capital invested. \$19675.02

Gross income. 15238.95

Total cost, not including delivery. 5113.50

Net Income at platform \$10125.45





The average cost per ton, calculated from operating expenses alone, as taken from the table is \$1.156. The cost per ton is considerable higher when the total cost is used, the figure being \$1.40.

#### COMPRESSION PLANTS.

To have a basis of comparison, actual data on two motor driven ice plants, not operated in connection with the central station, but buying their power, has been selected. The tables given were taken from the Electrical World of May 4, 1911. They were originally a part of a paper presented before the Chicago section of the American Institute of Electrical Engineers by Augustus C. Smith, sales engineer of the Cataract Power and Conduit Company of Buffalo, New York.

The first plant, which is located in Buffalo, is a plate system of One hundred tons capacity, using pure spring water. A One hundred ton compressor is driven by a Two hundred horse power, three phase, twenty-five cycle, twenty-two hundred volt, induction motor; the auxiliaries being driven by small motors, ranging from two to seven and a half horse power. The power consumption per ton of ice is shown in the following table:-

#### Energy Consumption.

1910	Tons of Ice Monthly	Ice Daily	Max. H.P.	H.P. Hours.	Max. H.P. per Ton	H.P. Hrs. per Ton.
Jan.				10314		
Feb.	1420	50.7	145	98214	2.86	69.2



Mar.	1400	45.2	153	105845	3.38	75.6
Apr.	1168	38.9	139	78933	3.58	67.6
May.	1786	57.6	138	101798	2.40	57.0
June.	1037	34.6	278	120720	8.00	116.4
July.	2294	74.0	280	201791	3.78	88.0
Aug.	1800	58.1	290	209200	4.98	116.2
Sept.	2244	74.8	283	198157	3.78	88.3
Oct.	1115	36.0	149	117363	4.13	105.3
Nov.	1019	34.0	141	98320	4.14	96.5
Dec.	1356	43.7	139	104398	3.19	77.0
	<u>16639</u>			<u>1445053</u>		Av. 86.8

The large values of energy consumption, noted in the table, are, more than likely, due to the compressor and motor being operated at much below their rated load. The assumption has been made that the power cost is two cents per kilo-watt hour, and at this rate the average cost per ton is \$1.30.

The second plant is also located in Buffalo, New York, but it is a One hundred ton, can system, using distilled water. Two Eighty-five horse power horizontal tubular boilers are used to furnish steam for part of the auxiliaries, and to supply steam for the distilled water. Two compressors, each driven by a One hundred and seventy-five horse power, three phase, twenty-five cycle, twenty-two hundred volt, induction motor, are used. The energy consumption per ton is given in the following table:-

#### Energy consumption.

1910	Tons of Ice		Max.	H.P.	Max. H.P.	H.P. Hrs.
	Monthly	Daily	H.P.	Hours.	per Ton	per Ton.
Jan.	1768	57.0	123	87070	2.16	49.24
Feb.	1549	55.3	137	79450	2.48	51.29
Mar.	1903	61.4	221	93760	3.60	49.27
Apr.	2732	91.1	232	164558	2.55	60.23
May.	2651	25.5	257	165488	3.01	62.42
June.	3024	100.8	300	188666	2.98	62.39
July.	3442	111.0	314	219265	2.83	63.70
Aug.	3503	113.0	300	208123	2.65	59.41
Sept.	3514	117.1	291	209027	2.49	59.48
Oct.	3379	109.0	283	185177	2.60	54.80
Nov.	982	32.7	137	88070	4.19	89.68





Dec.	<u>1853</u>	59.8	129	<u>93914</u>	2.16	<u>50.68</u>
	30300			1772568		Av. 58.50

Assuming the cost of power the same as in the first plant, the cost per ton is \$ .875.

An average of the cost per ton of the two plants is \$1.087. It must, however, be kept in mind that this cost takes nothing into account, except the power consumed. If the cost of labor, interest, insurance, taxes, and depreciation be taken into account the cost per ton will be considerably higher.

#### NATURAL ICE.

Data on the cost of natural ice is practically impossible to obtain, as the cost, shrinkage, ect., are rarely, if ever, determined. Therefore the cost, in a generally way only, can be found.

It is claimed by those who harvest natural ice that one hundred men at one dollar and a half per day can harvest from six to seven hundred tons per day, depending upon the quality and thickness of the ice. This gives an initial cost of from twenty to twenty-five cents per ton. Seldom is an ice house found at a point suitable for distribution, so hauling is necessary. It costs from fifty to seventy-five cents per ton to haul the ice to a distribution station or platform. Then there is insurance, taxes, and depreciation on buildings, which brings the cost of natural ice to about one dollar per ton.



V. CONCLUSIONS.

Cost of ice per ton at platform.

Theoretical compression system, Twenty ton, with Five hundred kilo-watt plant running compound condensing.	\$1.156
Theoretical compression system, Twenty ton, with One thousand kilo-watt plant, running compound condensing.	\$1.465
Theoretical compression system, Twenty ton, with Five hundred kilo-watt plant, running compound non-condensing.	\$1.330
Theoretical absorption system, Twenty ton, with Five hundred kilo-watt plant, running compound non-condensing.	\$1.345
Average.	<u>\$1.324</u>
Actual absorption system, Twenty ton, with Three hundred kilo-watt plant, running non- condensing, based on operating costs only.	\$1.156
Based on total costs.	\$1.400
Actual compression plate system, One hundred ton, power bought from central station.	\$1.300
Actual compression can system, One hundred ton, power bought from central station.	\$ .875
Average of plants buying power.	<u>\$1.087</u>
Natural Ice, approximately.	\$1.000





Every year marks an increasing demand for ice. This is largely due to economic causes, one of the main ones being that the standard of living in the United States is advancing every year. At the same time less natural ice is being used, first, because climatic conditions are making it harder to procure in some sections, and second, that, with the agitation for pure food a demand for pure ice is created. Also the winters in the United States are less severe than formerly, and the periods during which natural ice may be harvested are consequently shortened in the middle and southern states. The shortening of the harvesting period calls for more men to work for a shorter time. This presents a difficult problem to the men who harvest natural ice. Then the source of natural ice is rarely near the distribution point, hence it is necessary to transport the ice, usually by wagon. One more obstacle for the natural ice dealer, especially in the middle and southern states, is that some winters may be so mild that no ice can be harvested, therefore it is necessary to ship from a northern source, entailing greater expense.

For these reasons a large field is opened up to the manufacture of artificial ice. It can be made at any time, or continuously, therefore eliminating the necessity of a large number of men for a short period of time. It can be made at the point of distribution as easily, and as cheaply, as at a more remote point. The question of storage may, or may not, enter into the artificial ice proposition, but usually does. The storing of artificial ice eliminates the old method, which entailed much



loss by shrinkage due to saw-dust packing, because, at very little additional expense, the ice can be stored in a clean storage room kept at any temperature necessary by the same brine that freezes the ice.

Then it can be seen why, the field being opened up, there are many artificial ice plants to be found thru out the United States, successfully competing with natural ice.

Now to go one step farther, if the manufacturer of artificial ice can successfully compete with natural ice, as he certainly must do or he would not remain in business, why cannot the central station man compete even better when operating an ice plant directly in connection with his central station? The reply to this question is that he can, for he has a considerable part of his machinery already installed, and his office equipped so that his expenses will be a minimum. This point will now be proven by comparison of the theoretical plants and the actual data given.

A consideration of the results obtained from the calculations on the theoretical plants and from the actual data, show that the ice plant, no matter whether operated compression or absorption in connection with the central station, is a paying proposition. For the four cases calculated the average cost per ton at the platform is \$1.324, which compares favorably with the cost of \$1.40 as shown by the actual plant operated with the central station. When these figures are compared with the cost per ton of the two motor driven plants, buying power from the central station, it is seen that the central station man still





holds his own. The average cost of ice per ton in the two Buffalo plants, assuming two cents per kilo-watt hour to be the rate paid for power, is \$1.087. It should be remembered that this is based only upon power consumed. Taking into consideration the size of these plants, this compares favorably with the cost of \$1.156 per ton in the actual absorption plant when based only upon the operating cost. These figures show conclusively that the central station man can successfully compete with the artificial ice dealer and the natural ice man. If men, generating their own power, or even buying their power, can make a success, it stands to reason that the central station man can make money by installing an ice plant in connection with his central station.

Often the central station operator is desirous of increasing his load factor. This can be done by adding a motor load; why not have this load bring in greater profits by driving an ice plant? The load will be increased, and the efficiency of the power plant raised. The same power plant attendants can look after the ice machinery, and the only additional help necessary would be unskilled labor for handling the ice. Again, if he is operating at nearly rated capacity, he may wish to increase his returns. This may be done by adding an absorption system, that is if he is running his engines non-condensing. In this system his steam consumption will be increased somewhat, due to the back pressure on the engines caused by the generator. He will have a small load added due to motor driven auxiliaries.

In these calculations cases have been taken to show that the ice plant can be added successfully for different methods of





operation. If the plant is being run condensing the absorption system is out of the question, but a motor driven plant may be used to increase the load factor. In the case of a non-condensing plant, if the latter is operating sufficiently under its rated capacity, a motor driven plant may be added, or again, if it is operating near full capacity, an absorption plant may be used which will only increase the steam consumption a comparatively small amount, thus working the boilers somewhat harder. So it is seen that for nearly any condition of operation some solution can be offered which will bring profits to the central station management.

Therefore, the ice plant operated in connection with the central station is a paying proposition; for

There is an increasing demand for pure ice, with a decreasing demand for natural ice; and

The companies operating artificial ice plants, independent of the central station, are making a success; therefore

The central station man, operating the ice plant in connection with the central station, can successfully enter the field, as his expenses are a minimum, due to machinery already installed, and a competent operating corps at his command.



APPENDIX.





TABLE OF CONTENTS.

	page.
INTRODUCTION. . . . .	25
EFFICIENCY CURVE OF GENERATING UNITS. . . . .	26
STEAM CONSUMPTION CURVES OF ENGINES . . . . .	27
CASE I.	
Load Curve, First Season . . . . .	28
Table I. . . . .	29
Table II . . . . .	29
Load Curve, Second Season. . . . .	30
Table III. . . . .	31
Table IV . . . . .	31
Load Curve, Third Season . . . . .	32
Table V. . . . .	33
Table VI . . . . .	33
Load Curve, Fourth Season. . . . .	34
Table VII. . . . .	35
Table VIII . . . . .	35
CASE II.	
Load Curve, Second Season. . . . .	36
Table I. . . . .	37
Table II . . . . .	37
Load Curve, Third Season . . . . .	38
Table III. . . . .	39
Table IV . . . . .	39
Load Curve, Fourth Season. . . . .	40
Table V. . . . .	41
Table VI . . . . .	41
CASE III.	
Table I. . . . .	42
Table II . . . . .	42
Table III. . . . .	43
Table IV . . . . .	43
Table V. . . . .	44
Table VI . . . . .	44
Table VII. . . . .	45
Table VIII . . . . .	45
CASE IV.	
Table I. . . . .	46
Table II . . . . .	46
Table III. . . . .	47
Table IV . . . . .	47



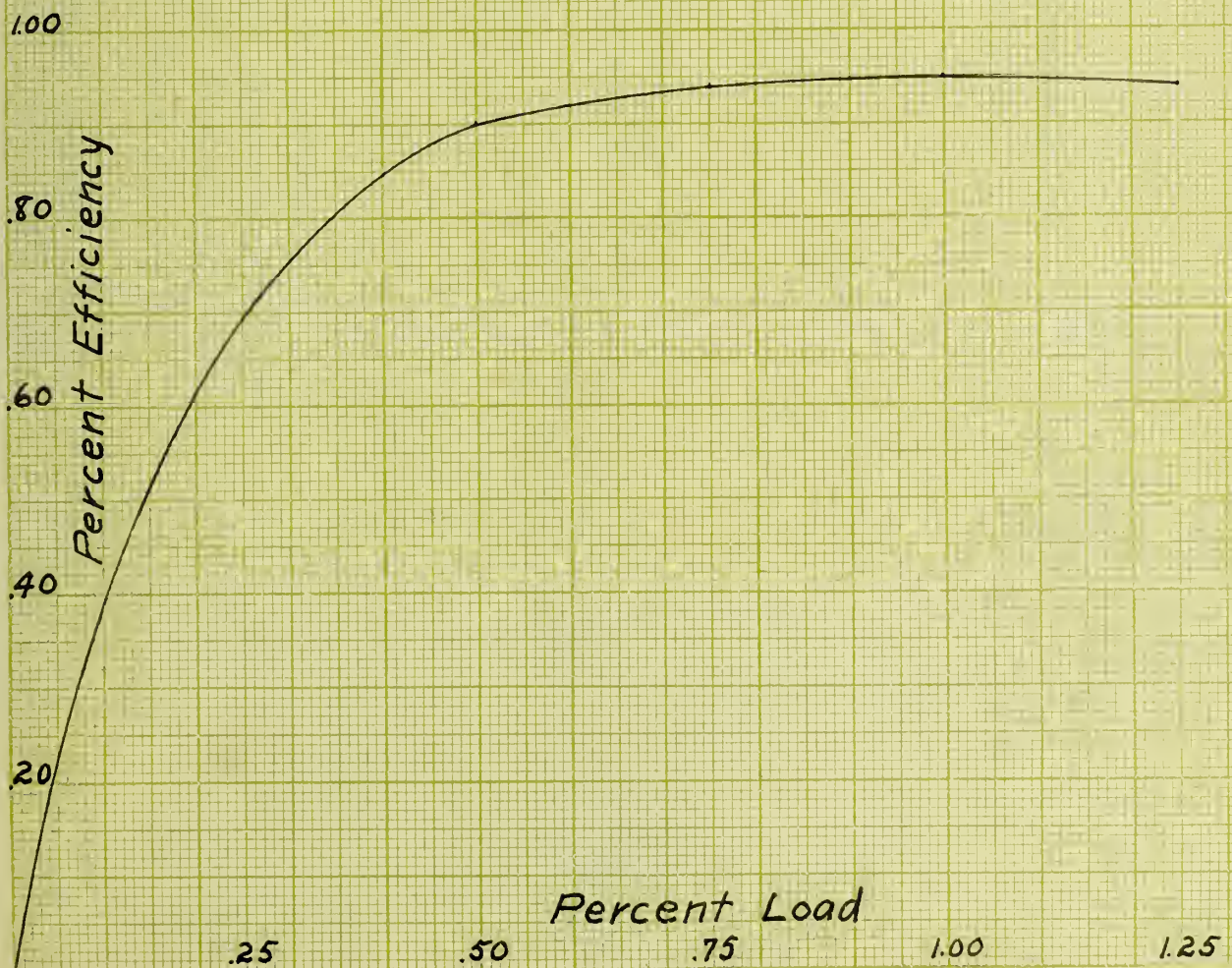
## INTRODUCTION.

In this appendix will be found the load curves and steam consumption tables for the various cases. For convenience each year has been divided into four divisions, or seasons, which very closely follow the seasons of the year. The same efficiency curve has been chosen for the various generating units, and a steam consumption curve has been taken for each of the different systems of operation. From the load curves assumed for each season the steam consumption has been calculated, and the results tabulated. In each case the engines have been assumed Ninety-two percent efficient, regardless of their load.

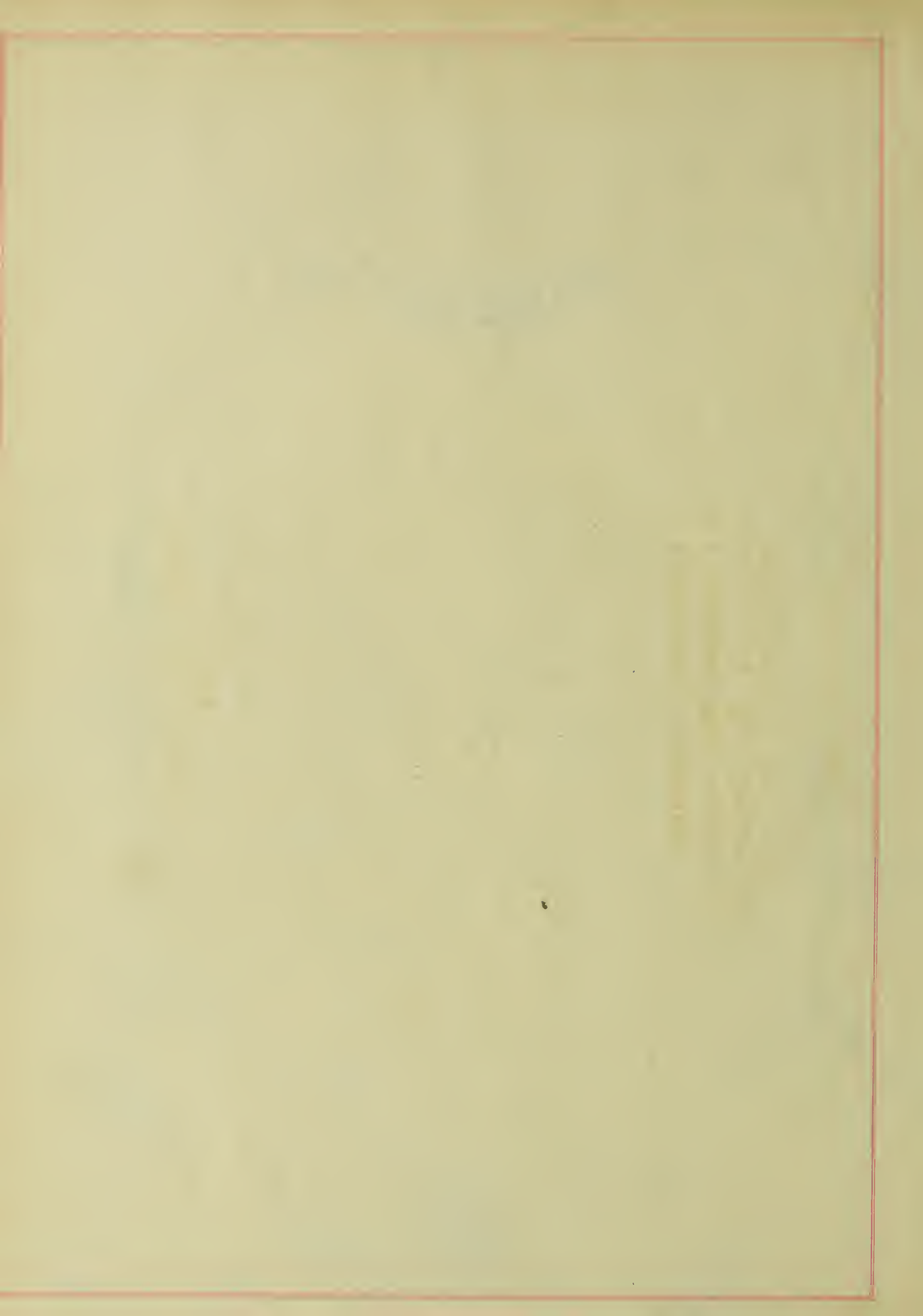




## Efficiency Curve For Generators







# Steam Consumption Curves

lbs. Steam Per I.H.P. Hr.

1. Compound Condensing
2. Compound Non-Condensing
3. Compound Non-Condensing With 2" Back Pressure.

Percent Load

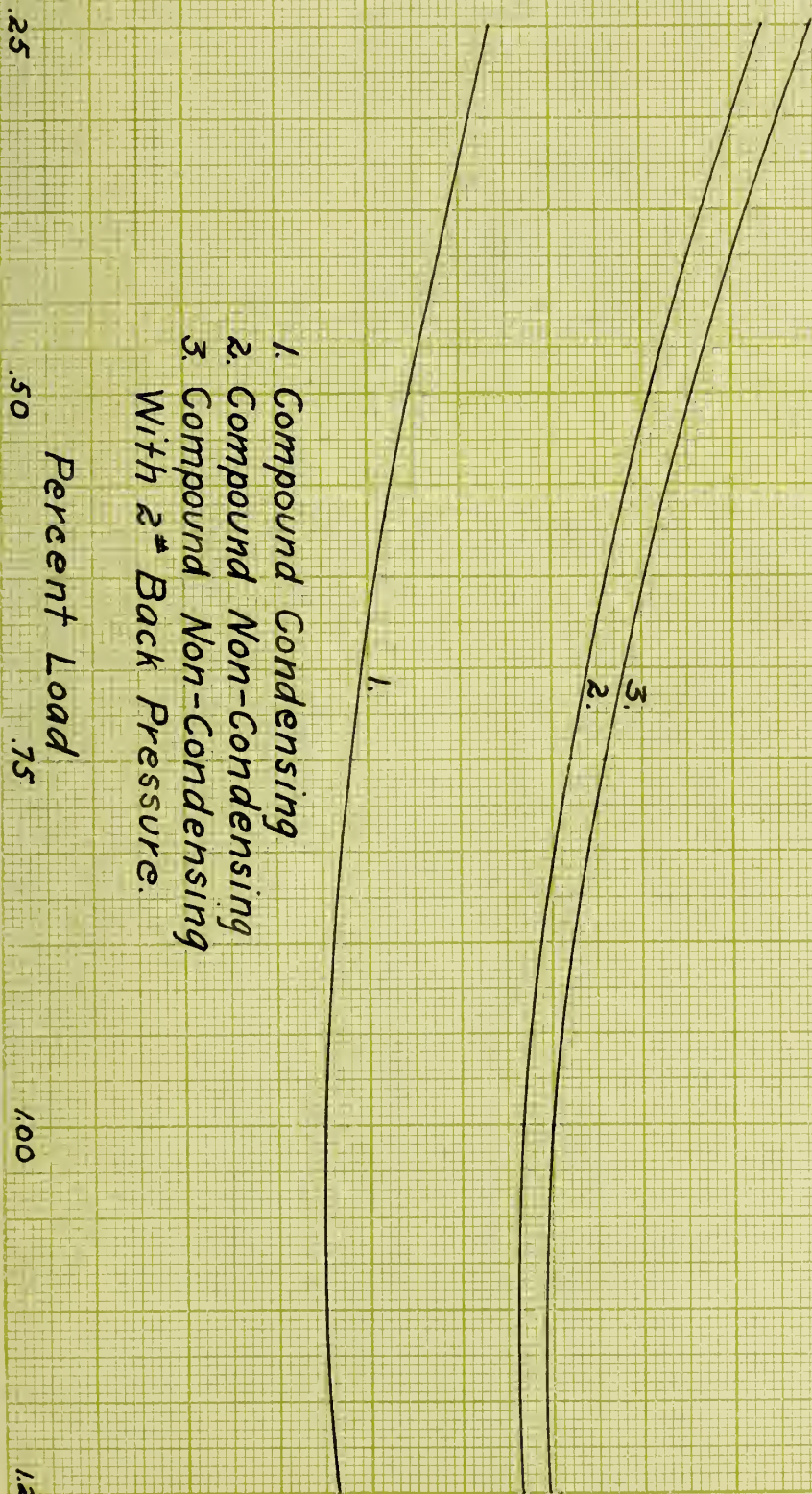
.25

.50

.75

1.00

1.25







Kilowatts

600  
500  
400  
300  
200  
100

Load Curve  
Case I  
First Season

Without Ice Plant  
With Ice Plant

12 2 4 6 8 10 12 2 4 6 8 10 12  
Time

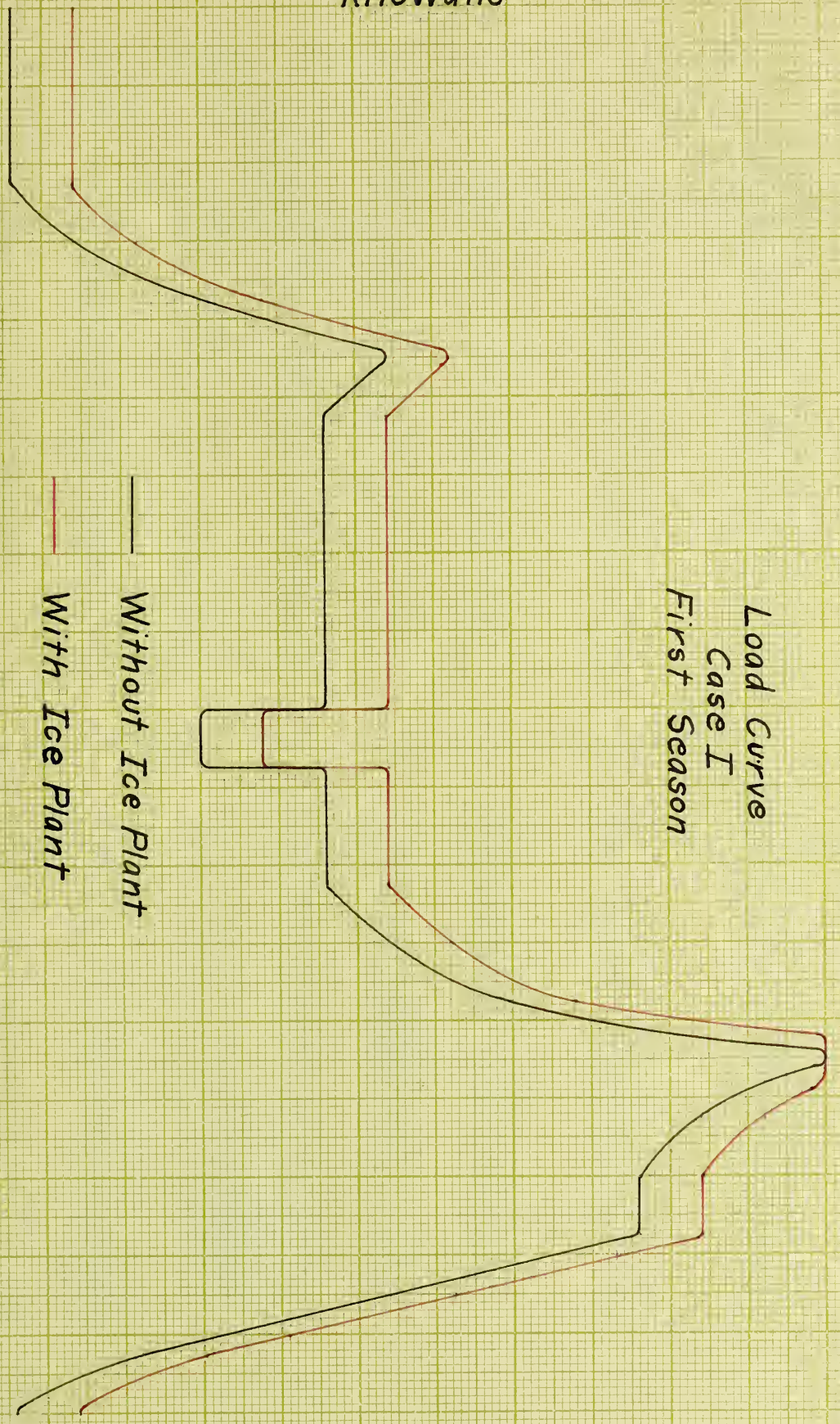






TABLE I. Steam Consumption without Ice-plant.

[illegible]

TABLE II. Steam Consumption with Ice-plant.

[illegible]





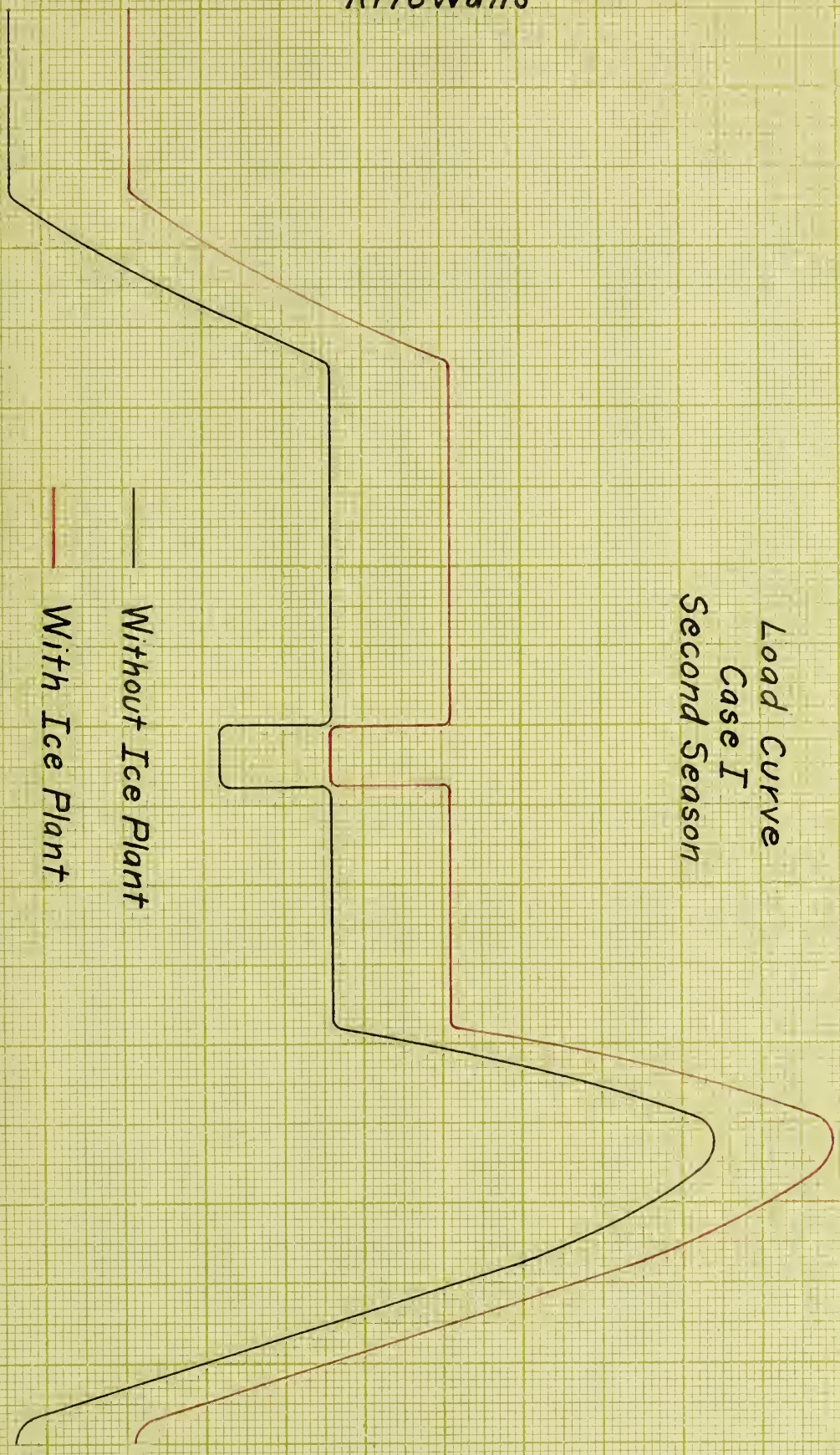
Kilowatts

600  
500  
400  
300  
200  
100

Load Curve  
Case I  
Second Season

Without Ice Plant  
With Ice Plant

Time  
12 2 4 6 8 10 12 2 4 6 8 10 12







				Input				# Steam	
% Load		Gen.	Eng.	Eng.	% Load		per	# Steam	
K.W.	Hr.	Gen.	Eff.	K.W.	B.H.P.	I.H.P.	Eng.	I.H.P. Hr.	Total
155	3	77.5	94.0	165	220	240	80.0	15.0	10800
175	1	87.5	95.0	184	246	268	89.2	14.5	3890
245	1	81.6	94.5	259	347	377	82.0	14.8	5580
315	1	105.0	95.0	332	445	484	105.0	14.0	6780
355	6	71.0	93.5	380	509	554	72.8	15.5	51500
285	1	57.0	91.5	311	419	455	60.0	16.8	7650
355	4	71.0	93.5	380	509	554	72.8	15.5	34400
435	1	87.0	94.5	460	616	670	86.0	14.5	9720
555	1	111.0	95.0	585	784	852	112.0	14.0	11920
575	1	125.0	94.0	612	820	891	117.0	14.1	12600
515	1	103.0	95.0	542	725	788	103.8	14.0	11100
415	1	83.0	94.5	440	590	641	84.4	14.8	9500
295	1	98.3	95.0	310	416	452	100.0	14.0	6330
195	1	97.5	95.0	205	274	298	99.3	14.0	4170
<u>24</u>									<u>185940</u>





Kilowatts.

600  
500  
400  
300  
200  
100

Load Curve  
Case I  
Third Season

Without Ice Plant  
With Ice Plant

12 2 4 6 8 10 12 2 4 6 8 10 12

Time

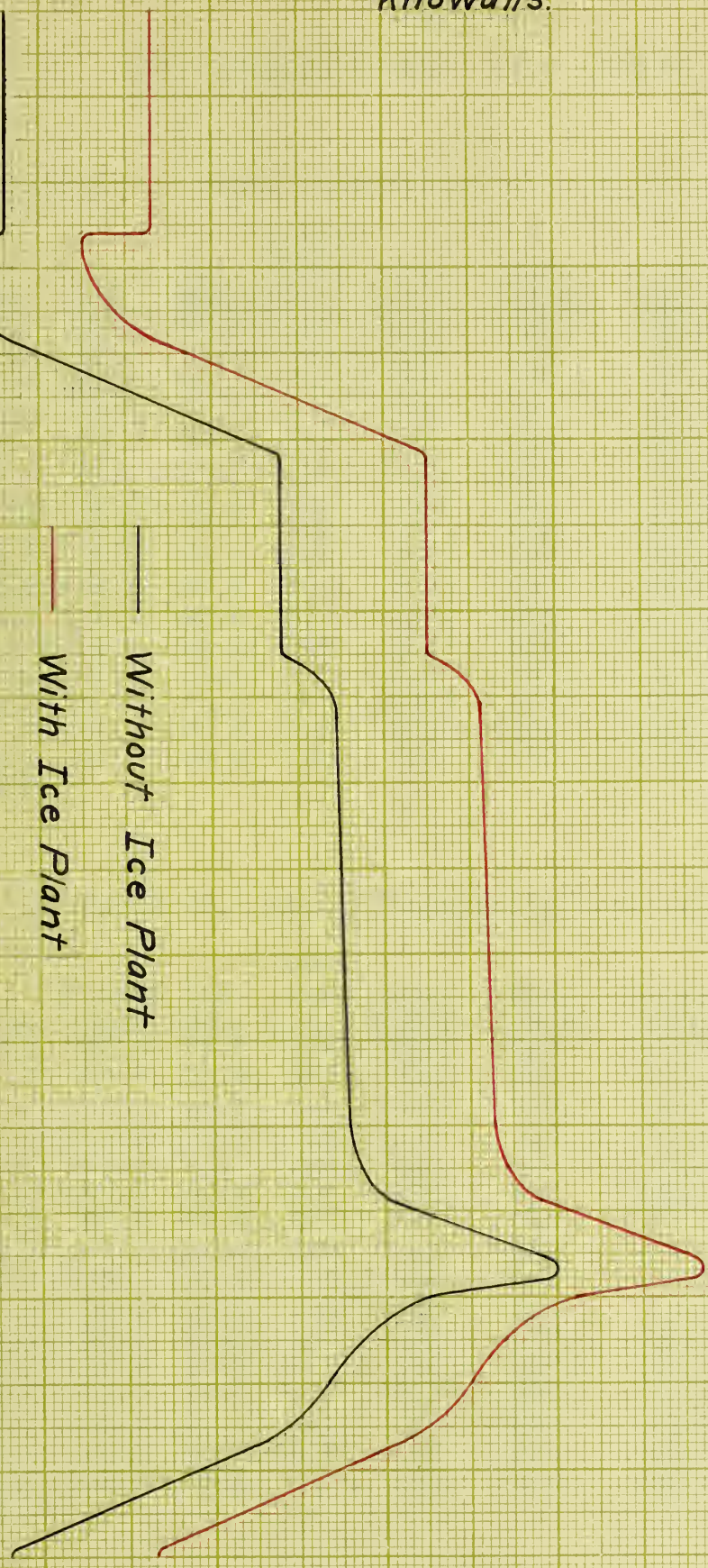






TABLE VI. Steam Consumption with Ice-plant.





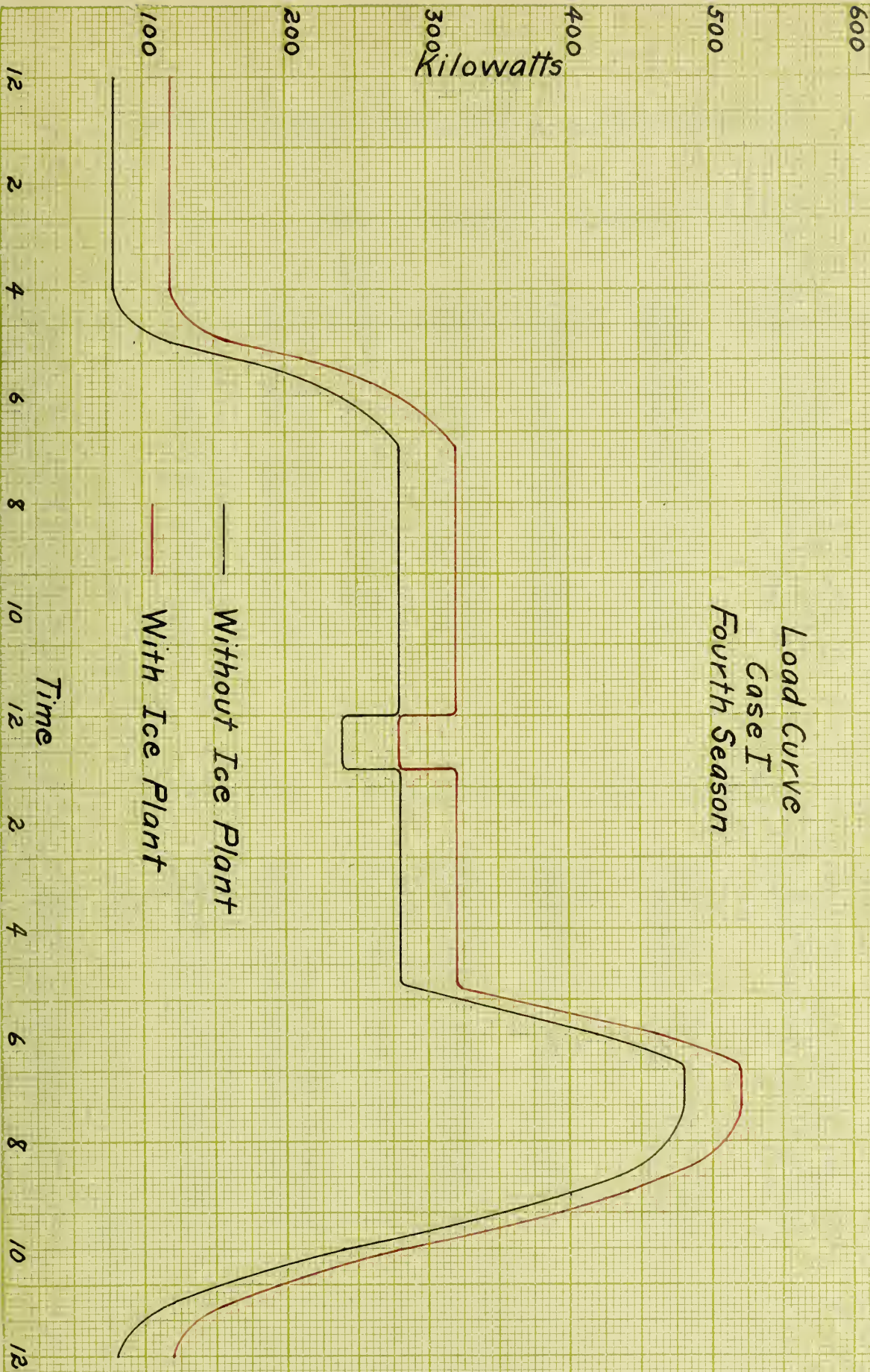






TABLE VII. Steam Consumption without Ice-plant.

TABLE VIII. Steam Consumption with Ice-plant.

[illegible]





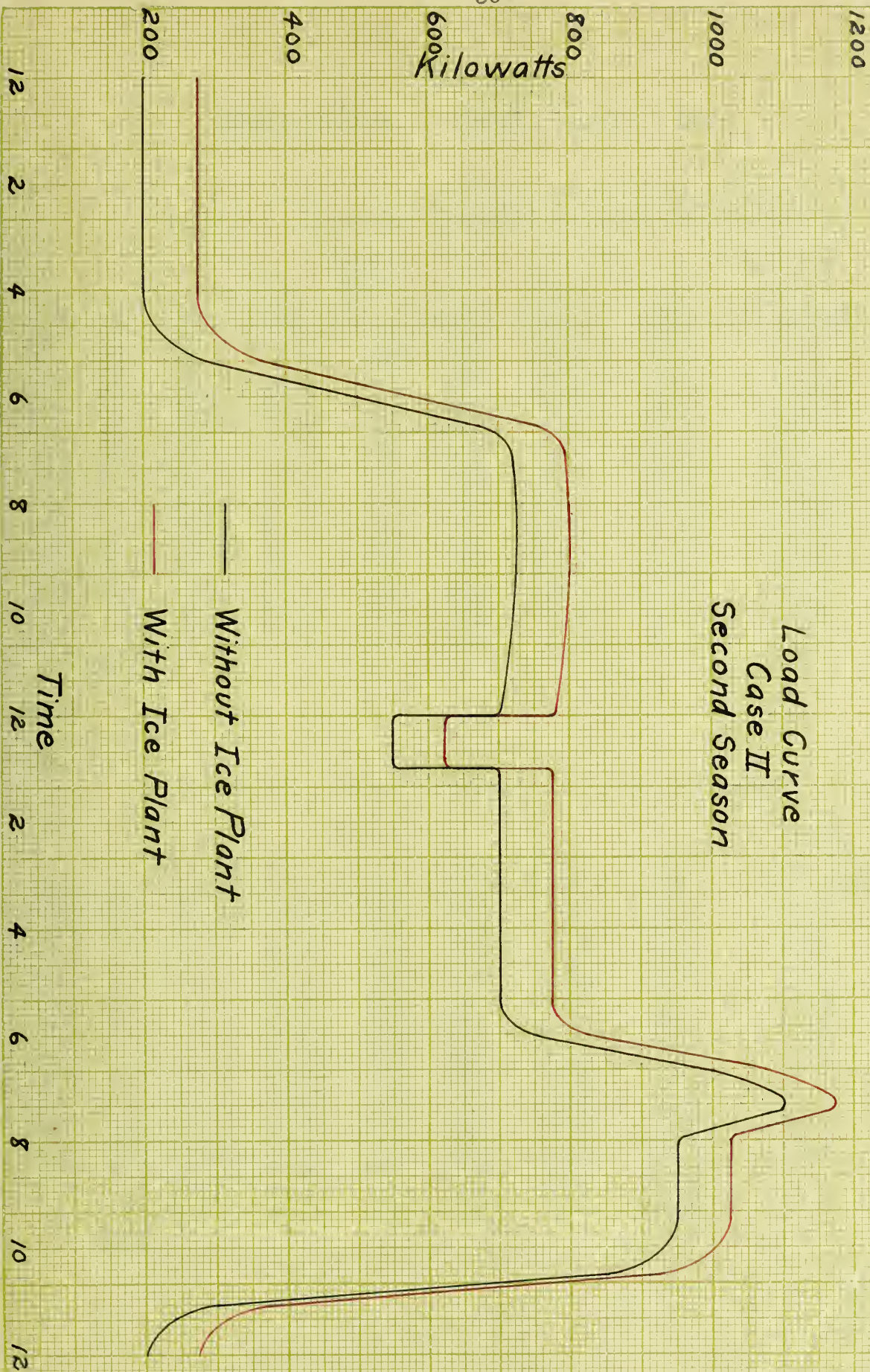






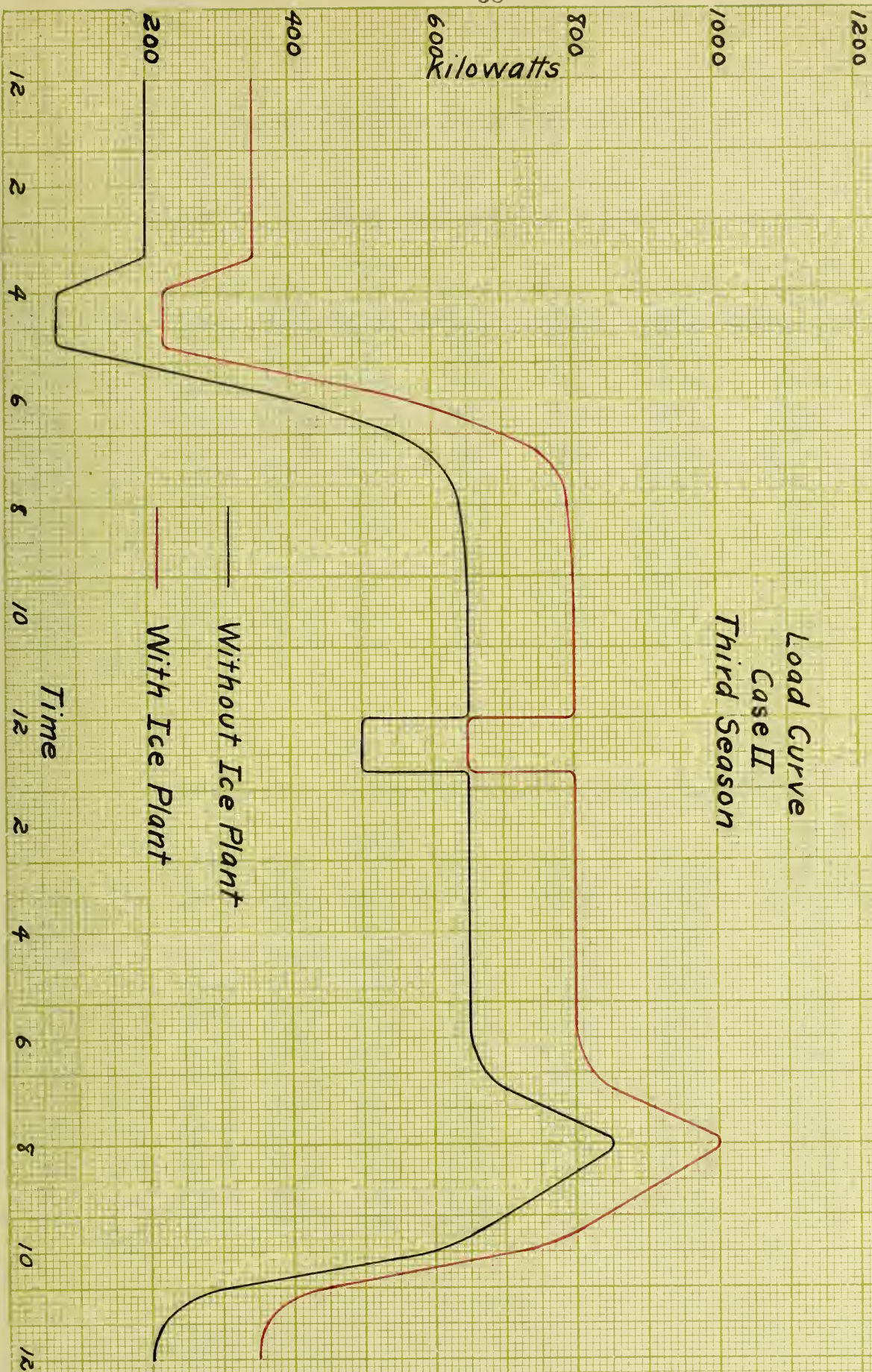
TABLE I. Steam Consumption without Ice-plant.

TABLE II. Steam Consumption with Ice-plant.

[illegible]







Load Curve  
Case II  
Third Season

Without Ice Plant  
With Ice Plant

kilowatts

Time

12 2 4 6 8 10 12 2 4 6 8 10 12

















TABLE V. Steam Consumption without Ice-plant.

TABLE VI. Steam Consumption with Ice-plant.

				Input			# Steam		
K.W.	Hr.	% Load Gen.	Gen. Eff.	K.W.	Eng. B.H.P.	Eng. I.H.P.	% Load Eng.	per I.H.P.	# Steam Hr. Total
275	4.5	91.6	95.0	290	388	422	91.7	14.2	26980
300	.5	100.0	95.0	316	424	461	100.0	14.0	3220
475	1.0	68.0	93.0	510	685	745	74.5	15.3	11400
775	1.0	77.5	94.0	825	1105	1200	82.5	14.9	17900
815	4.0	81.5	94.0	867	1162	1262	86.5	14.7	74400
800	1.0	80.0	94.0	851	1140	1240	85.0	14.8	18380
725	2.0	72.5	93.5	776	1040	1130	77.5	15.1	34150
785	4.0	78.5	94.0	835	1120	1220	83.5	14.9	72800
950	1.0	95.0	95.0	1000	1340	1460	100.0	14.0	20450
1125	1.0	112.5	95.0	1182	1582	1721	118.0	14.1	24300
985	1.0	98.5	95.0	1038	1390	1510	103.5	14.0	21150
975	1.0	97.5	95.0	1025	1372	1492	102.0	14.0	20900
950	1.0	95.0	95.0	1000	1340	1460	100.0	14.0	20450
575	1.0	82.0	94.0	612	821	894	89.4	14.5	12950
24.0									379430



### CASE III.





K.W.	Hr.	% Load		Input			% Load	# Steam	
		Gen.	Eff.	Gen.	Eng.	Eng.		I.H.P.	per
				K.W.	B.H.P.	I.H.P.	Eng.	I.H.P.	Total
155	3	77.5	94.0	165	220	240	80.0	24.0	17280
175	1	87.5	95.0	184	246	268	89.2	23.2	6220
245	1	81.6	94.5	259	347	377	82.0	24.0	9050
315	1	105.0	95.0	332	445	484	105.0	22.5	10880
355	6	71.0	93.5	380	509	554	72.8	25.0	83100
285	1	57.0	91.5	311	419	455	60.0	22.6	12100
355	4	71.0	93.5	380	509	554	72.8	25.0	55400
435	1	87.0	94.5	460	616	670	88.0	23.4	15680
555	1	111.0	95.0	585	784	852	112.0	22.4	19100
575	1	125.0	94.0	612	820	891	117.0	22.4	19980
515	1	103.0	95.0	542	725	788	103.8	22.5	16880
415	1	83.0	94.5	440	590	641	84.4	23.8	15260
295	1	98.3	95.0	310	416	452	100.0	22.6	10220
195	1	97.5	95.0	205	274	298	99.3	22.6	6750
24									297900



TABLE V. Steam Consumption without Ice-plant.





### CASE III.













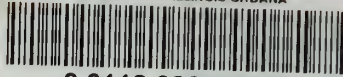








UNIVERSITY OF ILLINOIS-URBANA



3 0112 086828305